

## **SYNTHESIS OF NEW AROMATIC AZO-SCHIFF SULFONAMIDE DERIVATIVES AS CARBON STEEL ANTICORROSIVE IN 1 M HCL**

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### **Abstract:**

The synthetic sulfonamide derivative 4-((4-((4-chlorophenyl)imino)-2-hydroxypent-2-en-3-yl)diazonyl)benzenesulfonamide (HPDB) was studied using FT-IR, <sup>13</sup>CNMR, and <sup>1</sup>H NMR spectroscopy. Potentiometric polarization measurements were used to assess the inhibitory potential of the azo-azomethin molecule (HPDB). The presence of a physical adsorption process was corroborated by the thermodynamic features that were experimentally determined, and adsorption followed the "Langmuir" adsorption "isotherm". According to the electrochemical approach, raising the inhibitor concentration in 1M HCl solution enhanced the efficiency of the inhibition. It was also investigated how temperature affected the corrosiveness rate in the lack of and presence of these chemicals. For the dissolving process, the apparent activation energies, Arrhenius constant, enthalpies, and entropies were calculated and analyzed. The free energies and adsorption equilibrium constant were also found and discussed for the adsorption process. We gathered crucial knowledge regarding HPDB inhibitory behavior from the fundamental thermodynamic functions.

**Keywords:** Potentiometric, inhibitory, electrochemical.

### **Introduction**

Society suffers from corrosion, which is a major global problem for metallic materials [1]. "Mild" steel (MS) is among the most significant materials for maritime engineering, oil, gas, heat exchangers, tanks, network pipes, and water utilities because of its excellent electrical, thermal, and mechanical properties. In brackish or drinkable waters, MS is prone to natural corrosion in the presence of hostile ions like chloride (Cl<sup>-</sup>). Although hydrochloric acid (HCl) is a typical industrial cleaning, pickling, and descaling acid, it has harmful effects on metal surfaces due to its aggressive ions [2]. On the other hand, many industrial synthesis processes frequently use acids and salts [3]. Therefore, a suitable corrosion prevention strategy is needed to reduce different damages to the material and to preserve the economy. Corrosion inhibitors are essential as a result to prevent further harm to metallic components [4]. Numerous organic compounds with functional groups including -N=N-, -CHO, R-OH, and NH<sub>2</sub> were utilized as corrosion inhibitors in a variety of aqueous conditions. These compounds also had heteroatoms of nitrogen, sulfur, or oxygen [5]. A shielding layer is created on the metallic surface as a result



of these organic inhibitors adhering to it physically or chemically [6]. These two adsorption techniques provide a covering on the metal's surface that shields it from damaging ion bombardment [7]. Adsorption on a metallic surface causes organic inhibitors to react. Organic inhibitor molecules take the place of water molecules at metallic surfaces. When it comes to chemisorption, the anodic and cathodic processes are slowed down by the creation of a link between the metal and organic inhibitor, safeguarding the metal surface [8]. The effectiveness of these substances is heavily reliant on their capacity to form complexes with the metal since organic inhibitors work by adsorbing on the surface of the metal. Azo-azomethine Sulphonamides Derivatives are organic compounds that display great qualities that make them effective corrosion inhibitors, including the existence of heteroatoms with a single pair of electrons, numerous bonds (C=N, N=N), and aromatic rings [9]. Since the HCl environment is more corrosive than neutral or saline water settings, the chemicals used in this study were evaluated there rather than in those environments instead. Therefore, it is expected that the compounds investigated in this work will be acceptable corrosion inhibitors in less acidic conditions if they can tolerate the corrosiveness of HCl acid. In the investigation, various inhibitor concentrations and temperatures are taken into account.

## **2. EXPERIMENTAL**

### **2.1. "Materials" and synthesis of HPDB**

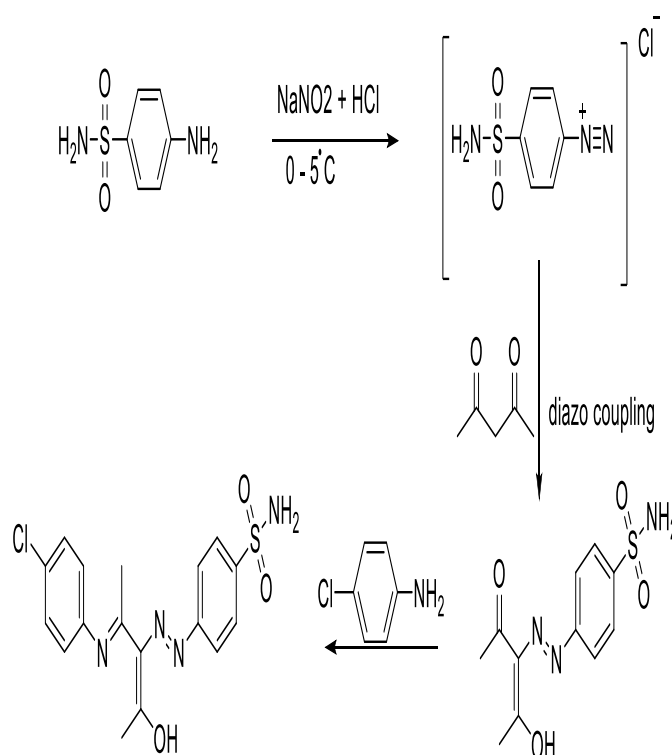
Original Content: Sourced from Fluka, our 4-chloroaniline and acetylaceton materials were top-notch. We also obtained HCl, NaNO<sub>2</sub>, Sodium carbonate, and sulphanilamide from the premium Sigma-Aldrich collection. No further purification was needed as we used analytical grade solvents, all thanks to Fluka. With precision in mind, we conducted our melting point measurements on the reliable Bauchi 510. As for our instrumentation, we meticulously recorded the compounds' solid-status FTIR spectra using KBr pellets and a Shimadzu FT-IR model 8400 S "Spectrophotometer". This covered a range of 4000 - 400 cm<sup>-1</sup>. Leveraging the power of a Bruker spectrophotometer (400 MHz), we investigated the <sup>1</sup>H NMR and <sup>13</sup>C NMR spectra with "DMSO-d<sub>6</sub>" using TMS as an internal standard and our solvent. The chemical was created using the approach outlined in the literature by Erdem et al [10]. Initially, 10 mL of 2N HCl were used to dissolve 5 mmol of sulfanilamide (0.86 g), which was then agitated until a clear solution was produced. "Sodium nitrate" (7.50 mmol, 0.50 g) was then gradually while stirring was added and lowering the temperature of the solution to 0–5°C. Stirring continued for a further 45 minutes after the addition was finished. Separately, 30 mL of an aqueous Na<sub>2</sub>CO<sub>3</sub> solution (20 mmol) was used to dissolve 0.5 g of acetylaceton (5 mmol), which was Afterwards, it was cooled in an ice bath to 0–5 °C. This combination was gradually added to the cold sulfanilamide diazonium salt solution. Another two hours were spent stirring at 0 to 5 degrees Celsius to maintain the pH at 6-7. The desired azo compound was obtained by recrystallizing the produced precipitate from ethanol after the precipitate had been manufactured. Through the use of thin-layer chromatography and an ethanol/chloroform (1:9) solvent system, the purity of the azo compound was evaluated. The fascinating and elaborate process of Schiff-base production, comprising a conventional condensation reaction, was



described. In this fascinating experiment, a balanced 1.0 mmol (0.28 g) of the alluring Azo compound and the 1 mmol of the alluring aniline derivatives were smoothly dissolved in a negligible amount of methanol. We cautiously added a few drops of glacial acetic acid to intensify the process, and we let it to reflux for exciting periods of 5 to 12 hours. The product's thrilling result was then painstakingly investigated using TLC in an acetone/chloroform (7:3) mixture. In an exciting process, A freezing temperature was reached after cooling the reaction mixture., resulting in the formation of pure compounds. This intriguing precipitate was then carefully filtered and washed, using cold absolute methanol, before being left to dry in open air. A fascinating variety of synthetic preparations for azo-azomethine compounds are brilliantly encapsulated in Scheme 1

76% yield, M.P.  $209 \pm 1^\circ\text{C}$ . The chemical was created, and the FTIR spectra (Fig. 1) revealed the subsequent bands of absorption.:  $1610\text{ cm}^{-1}$  (aromatic C=C),  $3228\text{-}3305\text{ cm}^{-1}$  ( $\text{NH}_2$ ),  $3479\text{ cm}^{-1}$  "(O-H)",  $1670\text{ cm}^{-1}$  "(C=N)" and  $1482\text{ cm}^{-1}$  "(N=N)". Additionally, the  $\text{SO}_2$  constituent may be seen in bands between  $1317\text{ cm}^{-1}$  and  $1153\text{ cm}^{-1}$ , which are the stretching vibrations of  $\text{SO}_2$  that are, respectively, asymmetrical and symmetric. [11,12].

Fig.2 shows  $^1\text{H}$ NMR spectra (400 MHz,  $\text{DMSO-d}_6$ ) with 6.96 - 8.02 ppm (m, 4H, Ar-H) ,12.05 ppm (s, 1H, OH). 6.94 ppm (m, 2H,  $\text{NH}_2$ ) and 5.91ppm (s, 6H,  $2\text{CH}_3$ ). 163 ppm (C=N), 179 ppm (C-O), 117-145 ppm (aromatic ring) and 27 ppm ( $-\text{CH}_3$ ) were found in  $^{13}\text{C}$ NMR spectra. Fig.3.



Scheme 1. Synthesis of (HPDB)





**2.2. Spaceman preparation**

The N-80 carbon steel sample that was employed in the experiment had a composition of 0.30% carbon, 0.050% phosphorus, 1.20% manganese, 0.060% sulfur, and iron as the final ingredient [13]. The mild steel surface was thoroughly cleansed with distilled water before each experimental test, washed with emery paper with a grit level of up to 1500, degreased with acetone, and then dried. Analytical grade 37% HCl was diluted to a concentration of 1M to create a hydrochloric acid solution. When the temperature fluctuated from 298, 308, and 318K and was set at ( $5 \times 10^{-4}$ ,  $1 \times 10^{-3}$ , and  $5 \times 10^{-3}M$ ), The variety of inhibitor concentrations that were used in this investigation changed.

**2.3. "Electrochemical" measurements**

Electrochemical evaluations were made utilizing a Bank ELEIKTRONKIK INTELLGENT CONTROLS Model Mlab 200 with a three-electrode configuration comprised of a mild steel working electrode [WE], a platinum counter electrode [CE], and a reference electrode[RE] made of a saturated calomel with Ag/AgCl. A 30-minute stabilization period was allowed prior to all electrochemical measurements to provide an open circuit potential that is steady-state. It was possible to produce potentiodynamic polarization curves by rate of scan  $1 \text{ mV s}^{-1}$  over a potential fluctuate of  $[-250 \text{ to } +250] \text{ mV (SCE)}$ [14]. The temperatures of  $[298 \text{ K}, 308 \text{ K}, \text{ and } 318 \text{ K}]$  were utilized to run all the test solutions

**3. RESULT AND DISCUSSION**

**3.1. Measurements of the potentiodynamic polarization**

Experiments were performed in 1 M HCl to comprehend how the resulting inhibitor, HPDB, affected carbon steel. Various doses of HPDB were used in potentiodynamic polarization studies at a range of temperatures between 298 and 318 K. Tafel slopes ( $\beta_a$  and  $\beta_c$ , respectively), for anodic and cathodic corrosion, as well as corrosion potential and current density, surface coverage ( $\theta$ ) and corrosion inhibition efficacy ( $\eta \%$ ) were among experimental findings. Table 1 displays these outcomes. It is crucial to remember that the surface coverage and the percentage of inhibition have a strong correlation with  $I_{\text{corr}}$  values and may be calculated using tried-and-true techniques. The section of the Tafle plots was extrapolated in order to get the corrosion current density ( $I_{\text{corr}}$ ). [15].

$$\% \eta = \left( \frac{I^{\circ}_{\text{corr}} - I_{\text{corr}}}{I^{\circ}_{\text{corr}}} \right) \times 100 \dots \dots \dots (1)$$

$$\theta = \left( \frac{I^{\circ}_{\text{corr}} - I_{\text{corr}}}{I^{\circ}_{\text{corr}}} \right) \dots \dots \dots (2)$$

the present study investigates the density of the corrosion currents, namely  $[I_{\text{corr}} \text{ and } I^{\circ}_{\text{corr}}]$ , in both "uninhibited" and "inhibited" states. The addition of hetero azo-azomethin group in HPDB serves as a potential inhibitor to reactive sites on mild steel surfaces. The experimental results demonstrate the density of the corrosion current reduces upon introduction of the inhibitor to aggressive media at constant temp. [16]. This study shows that a rise in inhibitor concentration corresponds due to a rise in  $I_{\text{corr}}$  concentration. Aside from that the increase in  $I_{\text{corr}}$  is caused by a rise in temperature. A approach of corrosion prevention is shown by the change in corrosion



potential ( $E_{corr}$ ) of the inhibitors in the blank solutions. Corrosion potential data of the HPDB inhibitor showed no significant changes on either the cathode or anode side, indicating that the corrosion inhibitor is of the mixed type. This conclusion is the cathodic ( $\beta_c$ ) and anodic ( $\beta_a$ ) slope values provide support, which showed little difference compared to the blank values. Previous studies by Haiduc et al. showed that An inhibitor falls within the category of [anodic/cathodic] if the anodic/cathodic side offset  $E_{corr}$  is significantly bigger than 85 Mv [17]. In the course of our research, it was discovered that the shift in  $E_{corr}$  values indicates that the HPDB inhibitor possesses the characteristics of a mixed-type inhibitor, with a range of less than 85 Mv. This observation provides a plausible explanation for the phenomenon that a decrease in temperature range resulted in lessening in inhibition efficacy, while an improvement in inhibitor concentration enhances inhibition effectiveness. As depicted in Figure 4, optimal conditions for HPDB in acidic media were determined to be 298 K and  $5 \times 10^{-3}$  M, corresponding to the lowest  $I_{corr}$  value of  $4.4 \text{ Acm}^2$  and the highest IE% value of 85.62. Notably, the introduction of the corrosion inhibitor HPDB was found to significantly lower the rate of corrosion, with the lowest rate of corrosion (CR) being recorded at the highest inhibit. The equations 3 that follow were used to determine the corrosion rate:

$$C.R \text{ in (mpy)} = 0.130 * I_{corr} * E.W / \rho \dots\dots\dots 3$$

E.W. : the metal's equivalent weight;  $\rho$  : the metal's density or alloy in ( $\text{g/cm}^3$ ).

Table 1 : In 1M HCl with varying HPDB concentrations, carbon steel corrosion polarization includes were detected.

Tem. K	Inh. Con. M	$E_{corr}$ mV	$I_{corr}$ $\mu\text{A}/\text{Cm}^2$	$\beta_a$ mv/Dec	$\beta_c$ mv/Dec	IE%	$\theta$	CR
298	blank	-461.1	30.6	296.9	-308.5	0	0	13.94
308		-464.1	35.6	362.0	-383.1	0	0	16.22
318		-441.7	39.2	328.1	-288.5	0	0	17.86
298	$5 \times 10^{-4}$	-465.3	11.0	129.5	-127.1	64.12	0.641	5.01
308		-454.1	16.3	127.1	-129.1	54.21	0.542	7.43
318		-456.8	19.8	174.1	-167.8	49.44	0.494	9.02
298	$1 \times 10^{-3}$	-466.7	6.9	92.1	-96.3	77.45	0.775	3.14
308		-450.4	9.6	135.1	-133.1	73.09	0.731	4.37
318		-449.9	11.6	110.7	-103.4	70.54	0.705	5.28
298	$5 \times 10^{-3}$	-460.2	4.4	147.3	-161.6	85.62	0.856	2.05
308		-417.1	7.7	89.1	-88.8	78.37	0.784	3.51
318		-439.7	9.1	128.6	-120.8	76.79	0.768	4.15



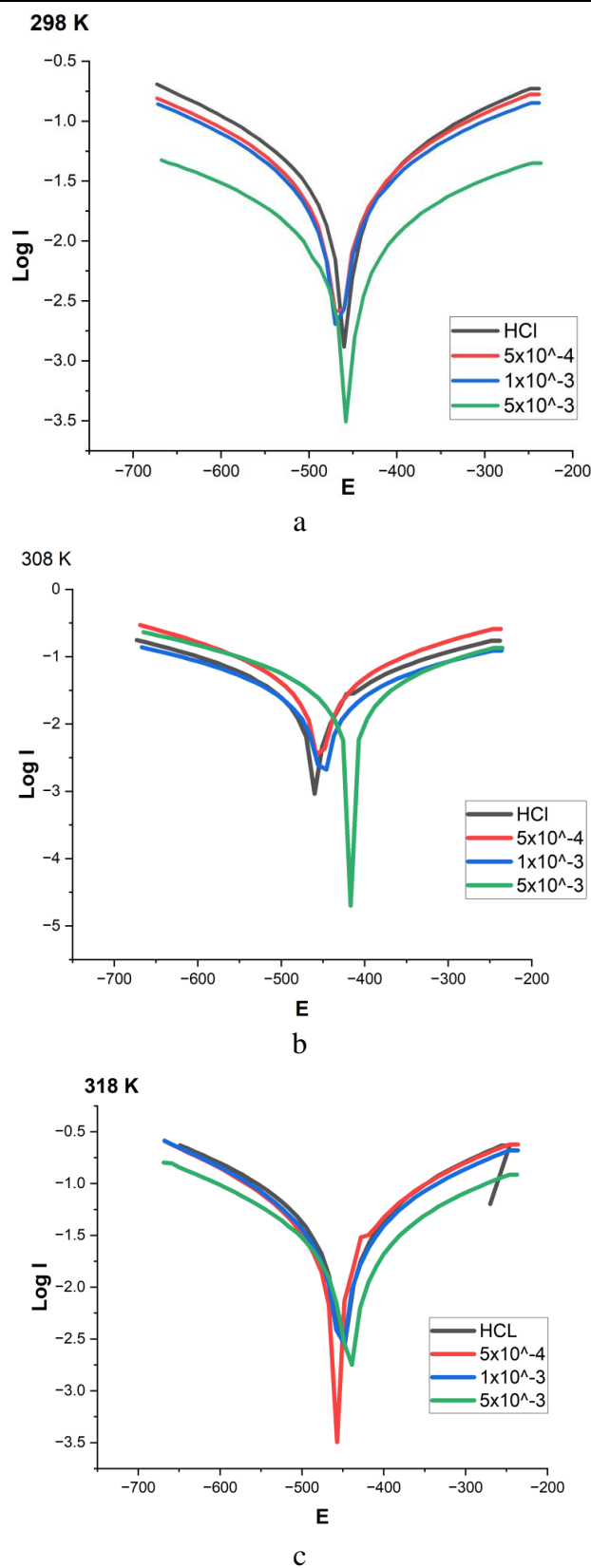


Fig. 4. Temperature-dependent potentiodynamic "polarization" graphs about carbon steel in 1 M HCl with and without HPDB (a) 298 K, (b) 308 K, and (c) 318 K.



### 3.2. Inhibitor Adsorption Isotherm Model

The examination of adsorption isotherm and thermodynamic parameters plays a significant part in comprehending the inhibition regarding organic molecules' role in the corrosion process. It is logical to investigate the process by which these molecules adhere to a surface made of metal. However, the majority of organic corrosion inhibitors' effectiveness is typically correlated with their ability to adsorb at the [metal/solution] contact. Possibly, this phenomena analyzed through isotherms of adsorption, which can offer further insight into the mechanism of "adsorption" such as the various of interactions between the steel and the inhibitory sector. In fact "corrosion" inhibitors can be adsorbed based on two different forms of interactions at the interface: the first; due to electrostatic interactions between charged molecules and the surface of the metal, physical adsorption (weak contacts)' the second; with electron sharing between inhibitors and iron d orbitals occurs during chemical adsorption. In the present investigation, the "Langmuir isotherm" of adsorption was employed as an explanation of nature that which adsorbs of azoazomethine "inhibitors" on the exterior of steel by adjusting covering the surface ( $\theta$ ) values for various HPDB concentrations, as outlined in eq.(3). [18]

$$\frac{C_{inh}}{\theta} = \frac{1}{K_{ads}} + C_{inh} \quad (3)$$

the adsorption equilibrium constant, denoted as  $K_{ads}$ , the coverage of surface, represented by  $\theta$ , and the concentration of the inhibitor, expressed as  $C_{inh}$ , are the variables of interest in this study. Figure 5 displays a linear relationship between  $C_{inh}/\theta$  and  $C_{inh}$  at varying temperatures. The intercept within the straight-lined with the y-axis determines the value of  $K_{ads}$  at various degrees of temperatures, accompanied by a "correlation" coefficient ( $R^2 \geq 0.999$ ) indicating high accuracy. Therefore, the inhibitor's adsorption on the surfaces of mild steel adheres to the Langmuire "adsorption isotherm" at all temperatures studied [19]. The chemical interaction's standard adsorption free energy change value is calculated using the equation below[20].

$$K_{ads} = \frac{1}{55.5} \exp\left(-\frac{\Delta G_{ads}}{RT}\right) \dots \dots \dots (4)$$

where the water's molar concentration is [55.5]. The global gas constant is R, and T stands for the absolute temp. According to these calculations, "Gibbs" free energy fluctuation is normally inversely correlated with  $K_{ads}$ , and the higher the negative value of  $G_{ads}$ , the more inhibitory molecules can be adsorbed. In addition, HPDB molecules are believed to be spontaneous. The mild steel surface was absorbed by the negative  $G_{ads}$  value[21]. The  $K_{ads}$  values in Table 2 also describe the extent of the combination of adsorbent and adsorbate. The  $K_{ads}$  content decreases with increasing temperature as the bond between the mild steel and the inhibitor molecules weakens. In addition, the  $G_{ads}$  value has been used in many studies to distinguish between chemisorption and physisorption processes. This process is called

Chemisorption occurs when the  $G_{ads}$  value is greater than -40 kJ/mol, as electrons are shared that exists between the metal and the inhibitor. The "physisorption" process, This entails the interaction of the inhibitor's charged metal surface with electrostatic forces., is believed to be possible when  $G_{ads}$  is greater than -20 kJ/mol[22]. As seen in Table 2, the  $G_{ads}$  information are between -31.2 and -32.2 kJ/mol. the adhesion of molecules of HPDB on metal surfaces is





believed to involve the processes of physisorption and chemisorption. In addition, the following equation illustrates how the "Van't Hoff" relationship was used to determine the enthalpy change of adsorption[23].

$$\text{Log } K_{\text{ads}} = \frac{-\Delta H_{\text{ads}}}{2.303 RT} + \text{Cons} \dots\dots\dots (5)$$

Here  $K_{\text{ads}}$  is adsorption's equilibrium value and  $H^{\circ}_{\text{ads}}$  is the heat of adsorption. Plot the logarithm of  $K_{\text{ads}}$  against  $[1/T]$  to determine the standard enthalpy (Figure 6). gave a line segment with a slope of  $[H^{\circ}_{\text{ads}} / R]$  according to the equation.(5). The inhibitor molecules are adsorbed exothermically on the surface of metal is represented by a negative  $H^{\circ}_{\text{ads}}$  value[24]. A negative  $H^{\circ}_{\text{ads}}$  result showed that the EI (%) decreased with increasing temperature. The significant value of  $H^{\circ}_{\text{ads}}$  (-17.81 kJ/mol) could Describe the gradual decrease in HPDB efficiency of inhibition with raising the temperature. This behavior can be explained as follows: At higher temperatures, there was increased desorption of inhibitory compounds deposited on the surface of the mild steel. The entropy value  $S^{\circ}_{\text{ads}}$  was positive, meaning that as the amount of inhibitor increased, the formation of the coated film became more ordered, or the reactants' reversal order increased towards the synthesis of Activated "complex". The adsorption entropy  $S^{\circ}_{\text{ads}}$  of the inhibitor can be determined use the equation below [25].

$$\Delta G^{\circ}_{\text{ads}} = \Delta H^{\circ}_{\text{ads}} - T \Delta S^{\circ}_{\text{ads}} \dots\dots\dots(4)$$

Table 2 contains a list of the obtained  $S^{\circ}_{\text{ads}}$  values.

Table 2 : Temperature-dependent thermodynamic characteristics of the generated inhibitor following its adsorption on a carbon steel surface in 1 M HCl

Com	T	R <sup>2</sup>	Log K <sub>ads</sub>	ΔG <sub>ads</sub> KJ.mol <sup>-1</sup>	ΔH <sub>ads</sub> KJ.mol <sup>-1</sup>	ΔS <sub>ads</sub> KJ.mol <sup>-1</sup>
HPDB	298	0.999	3.72	-31.206	-17.806	0.0449
	308	0.998	3.64	-31.748		0.0452
	318	0.999	3.53	-32.247		0.0459

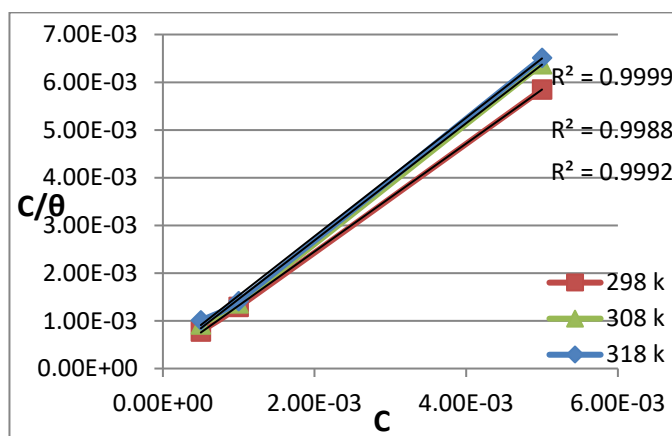


Fig. 5. An inhibitor HPDB adsorption model for the surface of carbon steel in 1 M HCl was created using the Langmuir isotherm.



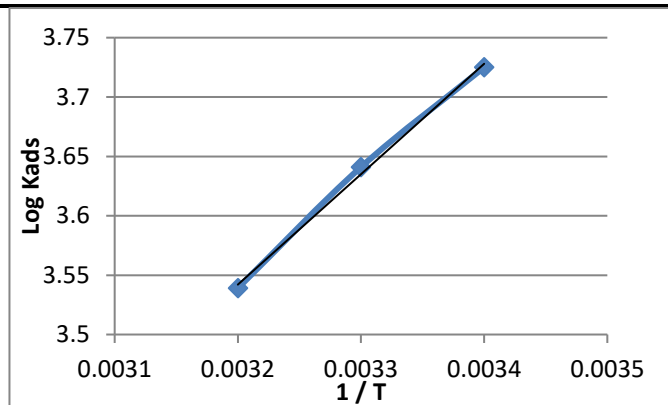


Fig. 6 : The correlation between [Log Kads and 1/T] for carbon steel in HCl solution of 1.0 M with various inhibitor quantities.

### 3.3 "Corrosion" kinetic and thermodynamic activation parameters

The influence temperature effects on corrosion rate of carbon steel in a 1.0 M HCl environment based on polarization curves in the range 298 to 318 K. The linear change in a measure of the corrosion current density's logarithm ( $i_{corr}$ ) as a consequence of the reciprocal in the presence of an inhibitor is depicted in Fig.6. of the temperature for a blank and in both situations. Examination for Explained by the activation parameters with and without inhibitor the mechanism of inhibitor "adsorption". The classic Arrhenius equation shown below may be used to compute the apparent activation energy ( $E_a$ ). [26].

$$\text{Log}(i_{corr}) = \text{Log} A - \frac{E_a}{RT} \dots \dots \dots (5)$$

Where  $R$  is the gas constant [ $E_a$ ] is the corrosion reaction's activation energy ( $\text{kJ mol}^{-1}$ ), In molecules  $\text{cm}^{-2} \text{s}^{-1}$ ,  $A$  is the preexponential factor., and  $T$  is the Kelvin-based absolute temperature.. Values for " $E_a$ " were calculated using the linear "slopes" of the connection between [ $\log(i_{corr})$  and  $(1/T)$ ] fig: 6. The "enthalpy" and entropy of the dissolution /passivation process were studied as activation parameters. [27]. The Formula for transition for the Arrhenius (equation (6)) can be used.

$$\log\left(\frac{i_{corr}}{T}\right) = \left[ \text{Log}\left(\frac{R}{hN}\right) + \left(\frac{\Delta S^*}{2.303R}\right) \right] - \frac{\Delta H^*}{2.303RT} \dots \dots 6$$

Where; The "temperature" is  $[T]$  in Kelvin terms, absolutely, The global gas constant is  $[R]$ . where  $[h]$  represents the Planck constant.  $[N]$  is Avogadro's number, ( $\Delta S^*$ ) is activation entropy  $\Delta H^*$  is the enthalpy of activation. The activation energy ( $E_a$ ) is shown in Table 3 , and of Carbon steel In the absence as well as the presence of various variables concentrations of (HPDB). Every value for ( $E_a$ ) exceeding the value in the blank. (12.44 kJ/mol), proving that (HPDB) retards the "Corrosion" response of Carbon steel [28]. A graph showing [ $\log(i_{corr}/T)$  vs  $(1/T)$ ] (Equation 6) results in a linear relationship, as illustrated in Figure 7, wherein Table (3)'s predicted values for the activation thermodynamic parameters [ $\Delta S^*$  and  $\Delta H^*$ ] and It has the following properties: [ $\log(R/hN) + (\Delta S^*/2.303R)$ ] as its intercept and a slope of [ $\Delta H^*/2.303R$ ]. The comparison of energy that activates in the raw state and in the subsistence of an inhibitor makes it possible to predict a temperature's impact concerning braking efficiency.



Radovici categorizes things in this way [29]. Conclusion: In our situation, the inhibitor has bonded to the steel surface via temperature-sensitive "electrostatic" bonds (weak bonds) [30]. Reduced correlation in braking efficiency as a temperature-dependent function with the shift of in the balance of adsorption and desorption. The positive enthalpy sign reflects the endothermic nature of the steel dissolution process. a rise in the entropy value as well signifies that as the chemicals afterwards become activated complexes in solution, there is a rise in disorder.

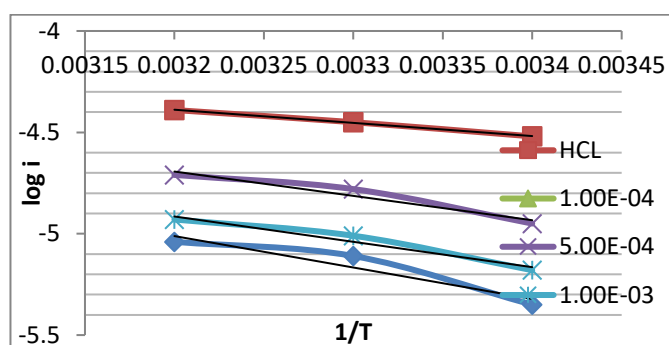


Figure 6. Plot  $[\log (i_{corr})]$  versus  $[(1 / T)]$  for carbon steel in 1M HCl with various doses of (HPDB) inhibitor.

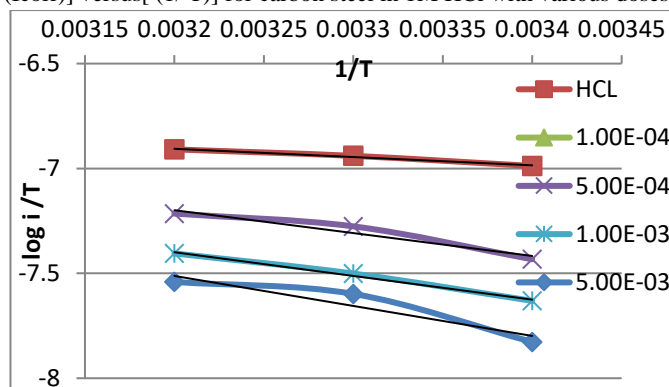


Figure 7 Plot  $\log (i_{corr}/T)$  versus  $[(1 / T)]$  for carbon steel in 1.0M HCl with various doses of (HPDB) inhibitor...

Table 3 Corrosion kinetic characteristics at different temperatures of a carbon steel surface in 1 M HCl of the produced inhibitor..

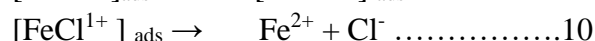
Com	$\Delta H^\ddagger$ KJ.mol <sup>-1</sup>	$\Delta S^\ddagger$ KJ.mol <sup>-1</sup> K	$E_a$ KJ.mol <sup>-1</sup>
blank	7.56	-0.305	12.44
5x10 <sup>-4</sup>	20.87	-0.268	22.97
1x10 <sup>-3</sup>	21.11	-0.271	23.93
5x10 <sup>-3</sup>	27.38	-0.253	29.67

#### 4. Suggestion of an inhibitory mechanism

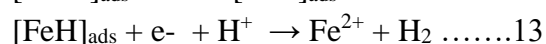
The mechanism of action of the inhibitors to preventing the (C.S) alloy from corroding in acidic solution (1M HCl) may be through absorbency of these inhibitions on the Carbon steel surface, forming an insulating layer that affects on the cathodic or anodic interaction or both of



them, and this Adsorption is influenced by the chemical constitution of these inhibitors in terms of the presence of heterogeneous atoms with high electronegativity such as (O, N, S ) and the bond electrons ( $\pi$ ) of aromatic rings through which the "inhibitor" adsorbs to the metal's surface., and these inhibitors are usually organic [31]. According to the results of the experimental results obtained from the various techniques used that were obtained , in 1.0 M HCl solution, the investigated organic dyes effectively prevent mild steel corrosion. previously published studies, the "mechanism" of inhibition The procedure with the tested organic molecules has been explored in detail Molecular Adsorption at the Metal/Solution Interface. The process of adsorption might take place physically, Chemically or a combination of the two adsorption types already discussed[32]. Physisorption: is a weak physical force of van der Waals adsorption or electrostatic interaction that occurs between the adsorbing surface and the adsorbed atoms or molecules or ions. The chlorine ion is first adsorbed on the external layer of the Carbon Steelalloy which carries a positive charge, as in the reaction (7), the molecules of the inhibitor are subsequently adsorbed during the electrostatic inter-action between the exterior of the negatively charged carbon Steel alloy ( $FeCl^-$ ) and the protonization inhibitor molecule of the positively charged, and in this way, form a layer protection that prevents the alloy from disintegration (anodic reaction) according to the reaction ( 7 – 10 ).



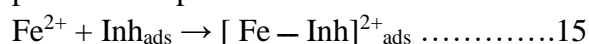
When hydrogen ions compete with the inhibitory molecules for adsorption on the alloy surface. According to the reaction (11–13), this results in a slower reaction rate and releases the hydrogen gas (cathodic reaction). [33,34].



Additionally, the process of adsorbing inhibitor molecules entails replacing one or more of the water molecules that were previously The inhibitor molecules or the anions of the acid medium are adsorbed on the metal surface.



where (x) denotes the water molecule count or size ratio that an organic inhibitor replaces with one. According to Equation (14), Possibly, the inhibitor molecules subsequently combine to produce metale inhibitor complexes with the freshly formed  $Fe^{2+}$ . Therefore, it makes sense to speculate that the presence of the chloride ion ( $Cl^-$ ) on the steel surface may encourage the positive complex to bind to the surface via electrostatic interactions. [35].



Chemisorption: is the formation of covalent or ionic bonds, coordinate bonds or a mixture thereof between the surface of the adsorbent and the adsorbed molecules, atoms or ions. Through a donor-acceptor contact (chemical adsorption), the electron pairs on the



heterogeneous oxygen, nitrogen, and sulfur atoms as well as the  $\pi$  electrons in the aromatic rings of the inhibitor molecules can adsorb. to adhere the particles to the surface, thus causing a chemical burn preventing substances from reaching the alloy surface, which reduces the corrosion rate [36,37].The studied inhibitory molecules are thought to be effective ligands because they can bind with metal ions to create coordination complexes[38]. Therefore, they can bind with the ions of  $Fe^{2+}$ , that develop on them create metal-inhibitor complexes [ $Fe^{2+}$  Inh.]ads on the steel surface, producing a block barrier for further resolution that corresponds with eq: 15.

## 5. CONCLUSION

For various concentrations, the inhibitory effectiveness was determined as a percentage of inhibitors in 1.0 M HCl as the corrosive medium at variousdegrees of temperatures by potentiodynamic polarization measurements. It has been observed that the percentage of inhibitory activity increases as increases inhibitor concentration at a fixed temperature and decreases when the temperature rises at a fixed concentration. The inhibitors tested functioned as mixed-type anodic-dominant inhibitors. Therefore, the high %IEs of achieved was interpreted as high organic molecule adsorption on mild steel surfaces with the tested inhibitors.. The Langmuir adsorption isotherm's prediction of this adsorption was proven to be accurate. HPDB adsorbs over the mild steel surface, and the fact that the Gibbs free energy of adsorption ( $G_{ads}$ ) is negative indicates the inhibitor compounds strongly contacted the mild steel surface.At  $5 \times 10^{-3}$  M concentration, the inhibition effectiveness was high (85.62%).

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