Physics and Chemical Method of Obtaining Extraction Phosphate Acid

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Abstract:

To obtain phosphate acid, natural phosphorites are affected by sulfuric acid in concentrates:

Ca5(PO4)3F + 5H2SO4 + 5nH2O = 5CaSO40nH2O + 3H3PO4 + HF

and in the next step, the method based on the extraction of sulfuric acid from the liquid phase is called an extraction or wet method. The resulting product is referred to as extraction phosphate acid (EFK). From the resulting phosphate acid, a variety of phosphorite fertilizers are developed. The main condition for the implementation of the process of acid extraction of sulfuric acid is the extraction of crystals from phosphate acid that are large enough of calcium sulphate, easily separated and well washed.

Introduction

During the extraction process, it must be possible to obtain a moving suspension of calcium sulfate in phosphate acid, mix it and transport it. When natural phosphate is directly mixed with concentrated sulfuric acid, a dark suspension is formed, which practically does not allow for separation into phases. To assist individuals desiring to benefit the worldwide work of Jehovah's Witnesses through some form of charitable giving, a brochure entitled Charitable Planning to Benefit Kingdom Service Worldwide has been prepared.

The concentration of additives is determined by both the raw material and the composition of the corresponding components, which are distributed between liquid, gas and solid phases. The presence of alkaline metal cations, magnesium, aluminum, iron cations and SO_{42-} , F⁻, SiF62 anion supplements in production solutions adequately changes the properties of sulfuric acid and product acid.

For the selection of the controlled and concentrated parameters of the extraction process, information about the limits of the existence of different modifications of calcium sulfate and the speed at which they become cohesive in phosphate acidic solutions is the basis. But in real solutions of extraction phosphate acid, the precise boundaries of the crystallization areas of plaster, calcium sulphate semicidration and angidrite and especially phase-by-phase conversion



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speeds vary sufficiently. For example, in pure solutions of phosphate acid containing 10-25% P 2O5, at 80 °C, most of the hemispherates are the first crystallizing phase of the system and become plastered for 1.5-2 hours. Such additives as iron phosphates, kremnezem can significantly intensify the process. The resulting gypsum can be present in metastabil (stable phase – angidritis) form for several days in solutions that hold P 2O5 for a few months and less than 25% in solutions that hold less than 10% P2O5. In accordance with the extraction conditions, liquid phase suspension is displayed in the form of metastabil digidrat, not stable angidritis, which is separated when it contains 25-30% P 2O5, temperature 70-80 oC, and mass staying in the reactor for 5-8 hours.

Accordingly, there are three methods of extracting phosphate acid: digidrate, semiconductor, and angidrite. The digidrate method is common, which is conducted at a temperature of $65-80^{\circ C}$ and contains between 30 and 32% P2O5 acid. It allows you to produce up to 50% P 2O5 in a semiconductor method carried out at a temperature of 90-105 $_{\circ C}$. The combined hemidrate-digidrate methods of extraction are becoming more widely dispersed, where semiconductor is first formed, and then, by diluting and cooling the suspension, it is re-crystallized into plaster. Such methods make it possible to obtain high-concentration (P 2O5 up to 50%) acid using raw materials effectively. The angidrid regime does not yet apply due to the high risk of corrosion of the equipment and the deterioration of filtration due to the difficulty of passing phosphate acid and washing solution through small crystals of calcium sulfate. Research is underway to address these challenges.

The shape and size of the calcium sulphate crystals produced by extraction determines the filtering properties of the sink layer, so its washing efficiency from phosphate acid depends on temperature and concentration of acidity, the level and conditions of degradation of the feeding. They also depend on the ratio of Ca²⁺ and SO₄₂ ions in the solution and the concentration of additives such as magnesium, aluminum, ftor compounds. When Ca²⁺ ions are redundant, the plaster is separated in a thin needle shape 20-80 mm long; When SO₄₂ ions are redundant, on the contrary, the size of plaster crystals reaches up to 100 inches wide and several hundred micrometers in height.

To obtain a large crystal-clear same-sex gypsum sink, the so₃:CaO molecular ratio in the liquid phase must be between 1.5 and 4.0 at the capacity level. When crystallizing semiconductor, it must be close to the stexiometric ratio, and in angidrite it is 10-15. In accordance with the modifications outlined, it is optimal to have SO $_3$ 1.5-2.5; 0.8-1.2%; 2.5-4.5%. It is necessary to ensure that the plaster crystallising is crystallized from as little saturated solution as possible. These conditions are provided by the intensive mixing of the suspension, its retsirculation (return to the initial component input part), the pre-mixing of sulphate and circular phosphate acids, and other instructions. In the digidrated method of extraction, on the contrary, high saturation is held, which has the ability to form pieces of compact spherical crystals.

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